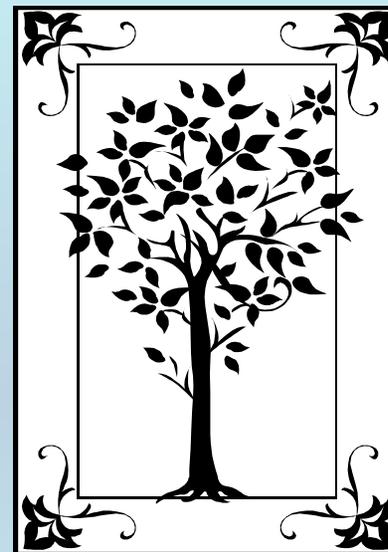


METADATA AND NUMERICAL DATA CAPTURE:

**Heat Capacities  $C_p$**

**(2 – Components)**

*Guided Data*  
**Capture (GDC)**



This tutorial describes  
METADATA AND NUMERICAL DATA CAPTURE:  
for **2-components**  
**Heat Capacities  $C_p$**   
with the Guided Data Capture (GDC) software.

## **NOTE:**

The tutorials proceed sequentially to ease the descriptions. **It is not necessary to enter *all* compounds before entering *all* samples, etc.**

Compounds, samples, properties, etc., can be added or modified at any time.

**However, the hierarchy must be maintained** (i.e., a property cannot be entered, if there is no associated sample or compound.)

The experimental data used in this example is from:

**Excess Molar Volume, Viscosity and Heat capacities for the Mixtures of Ethylene  
Glycol-Water from 273.15 K to 353.15 K**

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**Heat Capacities  $C_p$  for the binary system  
Ethylene glycol + water  
at  $p = 101.3$  kPa and various temperatures**

Table 5. The heat capacities for the ethylene glycol (1) + water (2)

| T/K    | $x_1$  |        |        |        |        |        |        |        |        |        |        |
|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|
|        | 0.0000 | 0.0312 | 0.0676 | 0.1105 | 0.1620 | 0.2248 | 0.3031 | 0.4036 | 0.5370 | 0.7230 | 1.0000 |
| 293.15 | 4.179  | 4.540  | 4.173  | 3.789  | 3.554  | 3.353  | 3.136  | 2.924  | 2.743  | 2.565  | 2.376  |
| 303.15 | 4.184  | 4.533  | 4.183  | 3.804  | 3.565  | 3.382  | 3.161  | 2.961  | 2.777  | 2.596  | 2.412  |
| 313.15 | 4.175  | 4.557  | 4.201  | 3.823  | 3.597  | 3.399  | 3.198  | 3.019  | 2.824  | 2.631  | 2.449  |
| 323.15 | 4.176  | 4.571  | 4.220  | 3.825  | 3.618  | 3.436  | 3.248  | 3.060  | 2.874  | 2.675  | 2.478  |
| 333.15 | 4.175  | 4.580  | 4.239  | 3.835  | 3.638  | 3.460  | 3.264  | 3.101  | 2.908  | 2.715  | 2.517  |
| 343.15 | 4.181  | 4.584  | 4.244  | 3.859  | 3.680  | 3.491  | 3.304  | 3.127  | 2.948  | 2.769  | 2.573  |
| 353.15 | 4.190  | 4.598  | 4.262  | 3.888  | 3.670  | 3.532  | 3.347  | 3.180  | 2.999  | 2.819  | 2.594  |
| 363.15 | --     | 4.603  | 4.268  | 3.901  | 3.718  | 3.568  | 3.396  | 3.214  | 3.043  | 2.851  | 2.658  |
| 373.15 | --     | --     | --     | 3.912  | 3.733  | 3.590  | 3.426  | 3.241  | 3.077  | 2.895  | 2.714  |

**This data set is  
considered here.**

## **Experimental Method & Uncertainties Info:**

**Method: DSC**

**Uncertainty: 1%**

The screenshot shows the 'Guided Data Capture - Thermophysical and Thermochemical Data' application. The menu bar includes 'File', 'Edit', 'Tools', and 'Help'. Below the menu is a tabbed interface with tabs for 'Reference', 'Compound', 'Sample', 'Mixture', 'Reaction', 'Property', and 'Data Tables'. The 'Property' tab is highlighted with a blue box. A blue arrow points from this tab to a yellow callout box containing the text '2. CLICK Property'. In the main tree view, the following structure is visible:

- 2003 yan ma 0
  - ethylene glycol
    - Sample 1 (cm;fd,mv;99.8m%,glc)
  - water
    - Sample 1 (cm::)
  - ethylene glycol + water

The 'ethylene glycol + water' entry is highlighted with a red box, and a red arrow points from it to a yellow callout box containing the text '1. SELECT the mixture for which the data are to be captured.'

**NOTE:** The **bibliographic information, compound identities, sample descriptions, and mixture** were entered previously. (There are separate tutorials, which describe capture of this information, if needed.)

Property and experimental method for ethylene glycol + water

Help

Property group: Heat capacity and derived properties

Property: Heat capacity at constant pressure Cp

Units: J/K/g

Method of measurement:

Experimental purpose:

1. SELECT the **Property Group**: *Heat capacity and derived properties*.

2. SELECT the **Property**: *Heat capacity at constant pressure Cp*.

3. SELECT the **Units**: *J/K/g*, here. **SELECT ALL OTHER UNITS** if another multiplier is needed.

OK

Cancel

**1. SELECT Method of Measurement** from the list provided. **NOTE:** *Other* can be a valid selection and should include a brief description in the **Comment** field.

Property: J/K/g

Method of measurement: Small sample (50 mg) DSC

Experimental purpose: Principal objective of the work

Comment (optional)

OK Cancel

**2. SELECT the Experimental Purpose** from the list provided.

**3. CLICK OK**

# SELECTION of # of Phases in Equilibrium and # of Constraints

Heat capacity at constant pressure  $C_p$  (J/K/g) as function of 2 variable(s)

Mixture: ethylene glycol + water

Phases in equilibrium:

1

Constraints:

1

Independent variables:

2

Phase of the Property Value(s)

SELECT the # of **Phases in equilibrium**. There is **1** phases; *liquid*.

**NOTE:** For “saturation conditions, this value would be 2; liquid & gas)

SELECT the # of **Constraints**. There is **1** constraint in the example; *pressure = 101.3 kPa*.

Heat capacity at constant pressure  $C_p$  (J/K/g) as function of 2 variable(s)

Mixture: ethylene glycol + water

Phases in equilibrium: 1 Constraints: 1 Independent variables: 2 Property set #: 1

Sample #: 1 Sample #: 1

Phase of the Property Value(s):

Definition of Measurement Results (Absolute vs Relative):

Data presentation: Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

Multiple *samples* for a given component can be accommodated, but this is rarely needed.

Heat capacity at constant pressure  $C_p$  (J/K/g) as function of 2 variable(s)

Mixture: ethylene glycol + water

Phases in equilibrium: 1 Constraints: 1 Independent variables: 2 Property set # 1 Sample # 1 Sample # 1

Phase of the Property Value(s) Liquid

Constraint 1 (Fixed value of) Liquid

Independent variable 1 Liquid

Independent variable 2 Liquid

Definition of Measurement Results (Absolute v. Relative)

**NOTE: Constraint and Independent Variable field(s) appear automatically based on the Gibbs Phase Rule.**

1) SELECT *Liquid* from the list provided for the **Phase of the Property Value**

# Specification of constraints, constraint values, and constraint units

1. SELECT the **Constraint(s)** ( $p$  here) and the **Independent Variable(s)** ( $T$  and  $x_1$ , here) from the lists provided.

ethylene glycol + water

Phases in equilibrium: 1 Constraints: 1 Independent variables: 2 Property set # 1 Sample # 1 Sample # 1

Phase of the Property Value(s) Liquid

Precision of the Property Value(s) 1 J/K/g %

Constraint 1 (Fixed value of)

Pressure Liquid Value: 101.3 Units: kPa Uncertainty: %

Independent variable 1

Temperature Liquid Units: K Uncertainty: %

Independent variable 2

Mole fraction of ethylene glycol Liquid Units: Dimensionless Uncertainty: %

Definition of Measurement Results (Absolute vs Relative)

2. TYPE the Constraint **Value** (*if required*) and SELECT **Units** for the Variable(s) and Constraint(s). Include **Uncertainties**, if known.

Property and method Numerical Data Cancel

# Measurement definition and Data presentation

Heat capacity at constant pressure Cp (J/K/g) as function of 2 variable(s)

Mixture: ethylene glycol + water

Phases in equilibrium: 1 Constraints: 1 Independent variable

Phase of the Property Value(s) Liquid

Constraint 1 (Fixed value of) Pressure of Liquid

Independent variable 1 Temperature of Liquid

Independent variable 2 Mole fraction of ethylene glycol of Liquid

Units: Dimensionless Uncertainty: %

Definition of Measurement Results (Absolute vs Relative)  
Direct value

Data presentation  
Experimental values

Comments (Optional):

Property and method Numerical Data Cancel

1. SELECT *Direct Value* (as compared with *Relative Value*) from the list defining the **Measurement Results**

2. SELECT the appropriate **Data presentation** method. *Experimental values* here.

3. CLICK *Numerical Data*

Heat capacity at constant pressure Cp (J/K/g) as function of

File Edit Action Help

|   | Var 1 | Var 2 | Property |
|---|-------|-------|----------|
| 1 |       |       |          |

**TYPE, or much preferably, PASTE the variable and property values into the table. See next page...**

**Table 5. The heat capacities for the ethylene glycol (1) + water (2)**

| T/K    | x <sub>1</sub> |        |        |        |        |        |        |        |        |        |        |
|--------|----------------|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|
|        | 0.0000         | 0.0312 | 0.0676 | 0.1105 | 0.1620 | 0.2248 | 0.3031 | 0.4036 | 0.5370 | 0.7230 | 1.0000 |
| 293.15 | 4.179          | 4.540  | 4.173  | 3.789  | 3.554  | 3.353  | 3.136  | 2.924  | 2.743  | 2.565  | 2.376  |
| 303.15 | 4.184          | 4.533  | 4.183  | 3.804  | 3.565  | 3.382  | 3.161  | 2.961  | 2.777  | 2.596  | 2.412  |
| 313.15 | 4.175          | 4.557  | 4.201  | 3.823  | 3.597  | 3.399  | 3.198  | 3.019  | 2.824  | 2.631  | 2.449  |
| 323.15 | 4.176          | 4.571  | 4.220  | 3.825  | 3.618  | 3.436  | 3.248  | 3.060  | 2.874  | 2.675  | 2.478  |
| 333.15 | 4.175          | 4.580  | 4.239  | 3.835  | 3.638  | 3.460  | 3.264  | 3.101  | 2.908  | 2.715  | 2.517  |
| 343.15 | 4.181          | 4.584  | 4.244  | 3.859  | 3.680  | 3.491  | 3.304  | 3.127  | 2.948  | 2.769  | 2.573  |
| 353.15 | 4.190          | 4.598  | 4.262  | 3.888  | 3.670  | 3.532  | 3.347  | 3.180  | 2.999  | 2.819  | 2.594  |
| 363.15 | --             | 4.603  | 4.268  | 3.901  | 3.718  | 3.568  | 3.396  | 3.214  | 3.043  | 2.851  | 2.658  |
| 373.15 | --             | --     | --     | 3.912  | 3.733  | 3.590  | 3.426  | 3.241  | 3.077  | 2.895  | 2.714  |

Clear the Table View plot Accept Cancel

Heat capacity at constant pressure  $C_p$  (J/K/g) as function of 2 variable(s)

File Edit Action Help

|    | Var 1  | Var 2  | Property |
|----|--------|--------|----------|
| 1  | 293.15 | 0.0000 | 4.179    |
| 2  | 303.15 | 0.0000 | 4.184    |
| 3  | 313.15 | 0.0000 | 4.175    |
| 4  | 323.15 | 0.0000 | 4.176    |
| 5  | 333.15 | 0.0000 | 4.175    |
| 6  | 343.15 | 0.0000 | 4.181    |
| 7  | 353.15 | 0.0000 | 4.190    |
| 8  | 293.15 | 0.0312 | 4.540    |
| 9  | 303.15 | 0.0312 | 4.533    |
| 10 | 313.15 | 0.0312 | 4.557    |
| 11 | 323.15 | 0.0312 | 4.571    |
| 12 | 333.15 | 0.0312 | 4.580    |
| 13 | 343.15 | 0.0312 | 4.584    |
| 14 | 353.15 | 0.0312 | 4.598    |
| 15 | 363.15 | 0.0312 | 4.603    |
| 16 | 293.15 | 0.0676 | 4.173    |
| 17 | 303.15 | 0.0676 | 4.183    |
| 18 | 313.15 | 0.0676 | 4.201    |
| 19 | 323.15 | 0.0676 | 4.220    |
| 20 | 333.15 | 0.0676 | 4.239    |
| 21 | 343.15 | 0.0676 | 4.244    |
| 22 | 353.15 | 0.0676 | 4.262    |
| 23 | 363.15 | 0.0676 | 4.268    |
| 24 | 293.15 | 0.1105 | 3.789    |
| 25 | 303.15 | 0.1105 | 3.804    |

Table 5. The heat capacity  $C_p$  (J/K/g) of ethylene glycol (1) + water (2)

| T/K    | $x_1$  |        |        |        |        |        |        |        |        |        |        |
|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|--------|
|        | 0.0000 | 0.0312 | 0.0676 | 0.1105 | 0.1620 | 0.2248 | 0.3031 | 0.4036 | 0.5370 | 0.7230 | 1.0000 |
| 293.15 | 4.179  | 4.540  | 4.173  | 3.789  | 3.554  | 3.353  | 3.136  | 2.924  | 2.743  | 2.565  | 2.376  |
| 303.15 | 4.184  | 4.533  | 4.183  | 3.804  | 3.565  | 3.382  | 3.161  | 2.961  | 2.777  | 2.596  | 2.412  |
| 313.15 | 4.175  | 4.557  | 4.201  | 3.823  | 3.597  | 3.399  | 3.198  | 3.019  | 2.824  | 2.631  | 2.449  |
| 323.15 | 4.176  | 4.571  | 4.220  | 3.825  | 3.618  | 3.436  | 3.248  | 3.060  | 2.874  | 2.675  | 2.478  |
| 333.15 | 4.175  | 4.580  | 4.239  | 3.835  | 3.638  | 3.460  | 3.264  | 3.101  | 2.908  | 2.715  | 2.517  |
| 343.15 | 4.181  | 4.584  | 4.244  | 3.859  | 3.680  | 3.491  | 3.304  | 3.127  | 2.948  | 2.769  | 2.573  |
| 353.15 | 4.190  | 4.598  | 4.262  | 3.888  | 3.670  | 3.532  | 3.347  | 3.180  | 2.999  | 2.819  | 2.594  |
| 363.15 | --     | 4.603  | 4.268  | 3.901  | 3.718  | 3.568  | 3.396  | 3.214  | 3.043  | 2.851  | 2.658  |
| 373.15 | --     | --     | --     | 3.912  | 3.733  | 3.590  | 3.426  | 3.241  | 3.077  | 2.895  | 2.714  |

Clear the Table View plot Accept Cancel

**NOTE:** Simple CUT/PASTE procedures can be used within the table to convert the original table into the required number of columns. (This can also be done externally in spreadsheet software, e.g., EXCEL.)

Heat capacity at constant pressure Cp (J/K/g) as function of 2 variable(s)

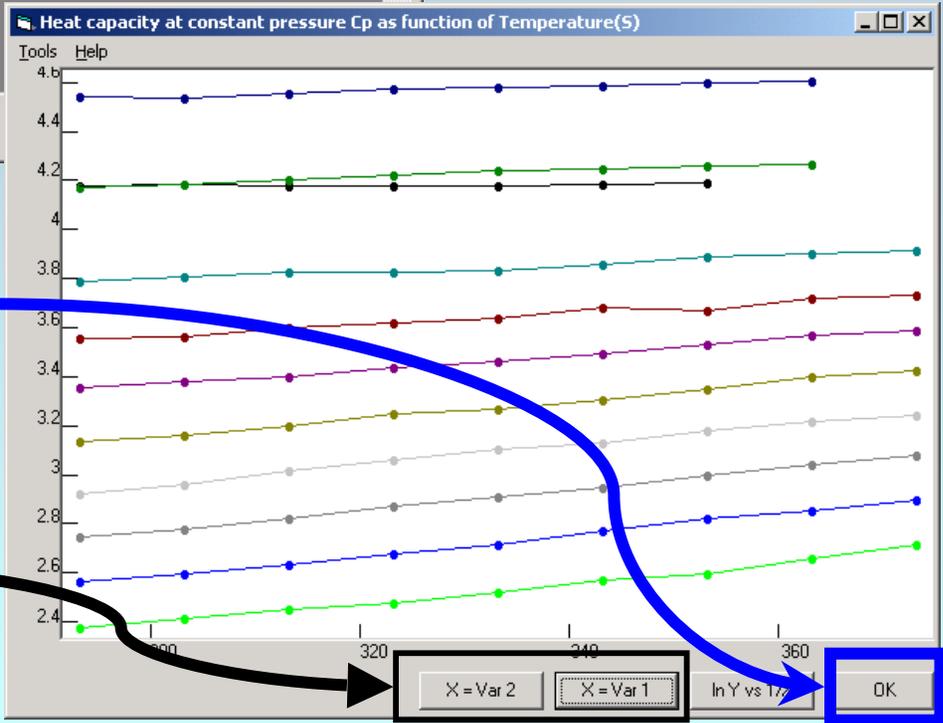
|    | Var 1  | Var 2  | Property |
|----|--------|--------|----------|
| 1  | 293.15 | 0.0000 | 4.179    |
| 2  | 303.15 | 0.0000 | 4.184    |
| 3  | 313.15 | 0.0000 | 4.175    |
| 4  | 323.15 | 0.0000 | 4.176    |
| 5  | 333.15 | 0.0000 | 4.175    |
| 6  | 343.15 | 0.0000 | 4.181    |
| 7  | 353.15 | 0.0000 | 4.190    |
| 8  | 293.15 | 0.0312 | 4.540    |
| 9  | 303.15 | 0.0312 | 4.533    |
| 10 | 313.15 | 0.0312 | 4.557    |
| 11 | 323.15 | 0.0312 | 4.571    |
| 12 | 333.15 | 0.0312 | 4.580    |
| 13 | 343.15 | 0.0312 | 4.584    |
| 14 | 353.15 | 0.0312 | 4.598    |
| 15 | 363.15 | 0.0312 | 4.603    |
| 16 | 293.15 | 0.0676 | 4.173    |
| 17 | 303.15 | 0.0676 | 4.183    |
| 18 | 313.15 | 0.0676 | 4.201    |
| 19 | 323.15 | 0.0676 | 4.220    |
| 20 | 333.15 | 0.0676 | 4.239    |
| 21 | 343.15 | 0.0676 | 4.244    |
| 22 | 353.15 | 0.0676 | 4.262    |
| 23 | 363.15 | 0.0676 | 4.268    |
| 24 | 293.15 | 0.1105 | 3.789    |
| 25 | 303.15 | 0.1105 | 3.804    |

Clear the Table View plot

1. CLICK *View plot* to see a graphical representation of the data.

2. Check for typographical errors, and CLICK *OK*, when done.

**NOTE:** The variable associated with the x-axis can be selected for best display.



Heat capacity at constant pressure Cp (J/K/g) as function of 2 variable(s)

File Edit Action Help

|    | Var 1  | Var 2  | Property |
|----|--------|--------|----------|
| 1  | 293.15 | 0.0000 | 4.179    |
| 2  | 303.15 | 0.0000 | 4.184    |
| 3  | 313.15 | 0.0000 | 4.175    |
| 4  | 323.15 | 0.0000 | 4.176    |
| 5  | 333.15 | 0.0000 | 4.175    |
| 6  | 343.15 | 0.0000 | 4.181    |
| 7  | 353.15 | 0.0000 | 4.190    |
| 8  | 293.15 | 0.0312 | 4.540    |
| 9  | 303.15 | 0.0312 | 4.533    |
| 10 | 313.15 | 0.0312 | 4.557    |
| 11 | 323.15 | 0.0312 | 4.571    |
| 12 | 333.15 | 0.0312 | 4.580    |
| 13 | 343.15 | 0.0312 | 4.584    |
| 14 | 353.15 | 0.0312 | 4.598    |
| 15 | 363.15 | 0.0312 | 4.603    |
| 16 | 293.15 | 0.0676 | 4.173    |
| 17 | 303.15 | 0.0676 | 4.183    |
| 18 | 313.15 | 0.0676 | 4.201    |
| 19 | 323.15 | 0.0676 | 4.220    |
| 20 | 333.15 | 0.0676 | 4.239    |
| 21 | 343.15 | 0.0676 | 4.244    |
| 22 | 353.15 | 0.0676 | 4.262    |
| 23 | 363.15 | 0.0676 | 4.268    |
| 24 | 293.15 | 0.1105 | 3.789    |
| 25 | 303.15 | 0.1105 | 3.804    |

**CLICK *Accept***

Clear the Table View plot Accept Cancel

## Guided Data Capture - Thermophysical and Thermochemical Data

File Edit Tools Help

Reference

Compound

- [-] 2003 yan ma 0
  - [-] ethylene glycol
    - ... Sample 1 (cm;fd,my,99.8m%,glc)
  - [-] water
    - ... Sample 1 (cm::)
  - [-] ethylene glycol + water

^2: CP (Set 1), B Method:SDSC dCP=1%

**NOTE:** The new data set now appears in the tree under the appropriate *mixture*.

**NOTE:** DOUBLE CLICKING on the *data set* allows editing of all entered information.

**END**

**Continue with other compounds,  
samples, properties, reactions, etc...**

***or save your file and exit the program.***